

## Virtual Formulation Laboratory

### for prediction and optimisation of manufacturability of advanced solids based formulations Powder Flow 2018: Cohesive Powder Flow

organised by

Formulation Science and Technology group (FSTG) of the Royal Society of Chemistry

12 April 2018 Burlington House, London

# Academic Collaborators



Engineering and Physical Sciences Research Council

**Imperial College** 

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Csaba Sinka, Ruslan Davidchack, Ben Edmans, Nicodemo Di Pasquale

University of Leicester

- Mojtaba Ghadiri, Xiaodong Jia, Mehrdad Pasha University of Leeds
- Mike Bradley, Rob Berry, Pablo Garcia Trinanes, Baldeep Kaur

University of Greenwich

• Jerry Heng, Vikram Karde Imperial College







# Industrial Partners



**EPSRC** Engineering and Physical Sciences

Research Counci

Imperial College

- Centre for Process Innovation (CPI)
- Procter & Gamble
- GlaxoSmithKline
- AstraZeneca
- Nestle
- KP Snacks
- Chemours

- Malvern Instrument
- Brookfield
- Britest
- Process Systems Enterprise (PSE)
- Griffiths Food
- Freeman Technology
- DEM Solutions







# VFL: 4 Processes/ 4 Problems









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Dr Nicodemo Di Pasquale and Prof. Ruslan Davidchack

- Prediction of Adhesive Interactions by Molecular  $\bullet$ dynamics (MD), using Cleaving Method
- Comparison of results from MD simulation with FD-IGC experimental work at ICL







### London Surface Energy Characterisation using Inverse Gas Chromatography (FD-IGC) Dr Vikram Karde and Dr Jerry Heng



Surface energy determination using IGC



Anisotropy in crystalline solids (Heterogeneous surfaces)





Facet specific surface energy using Contact angle

Surface energy heterogeneity using Finite Dilution IGC (FD-IGC)



Surface Coverage (%) Surface energy heterogeneity profile











### Flowability, Mixing, Segregation Dr Mehrdad Pasha, Dr Xiaodong Jia and Prof. Mojtaba Ghadiri



Single particle characterisation

Particle assembly behaviour prediction by DEM

**Experimental validation** 

VFL Toolkit development in a collaborative way

















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## Particle and Bulk Scale Measurements

Dr Pablo Garcia Trinanes, Dr Rob Berry and Prof. Michael Bradley • Particle size and shape measurement

- - G3 morphologi shape/ size
  - Air-swept sieve size
  - Pycnometer material density
- Bulk flow properties
  - Brookfield (PFT) freeman for high stress tests? flow function, friction, bulk density (voidage)
  - Uniaxial compaction test for high stress tests
- Segregation properties
  - Free surface (rolling segregation) for coarse particles > approx. 100 mm
  - Air induced (elutriation) for separation of fines (sub 50 mm) from wider distribution

### Caking properties

- Capability for measuring cake strengths driven by:
  - moisture migration, chemical reaction or plastic flow mechanisms in storage









### Work Plan of Leeds Flowability | Segregation | Mixing



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## Material Characterisation

#### Surface Adhesion

#### Method

- The powder will be dispersed into a flat target (material of interest) using Malvern G3 Morphologi disperser.
- The target will then be dropped from a range of heights until a satisfactory detachment of particles is observed by image analysis.
- Two images, before and after the drop, are taken by SEM to assess the detached and attached particles on the surface of the target

#### Calculations



 $R = \frac{\text{smallest detached particle} + \text{largest attached particle}}{2}$ 

# Schematic



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## Material Characterisation

Surface Adhesion















## Measurement of Surface Energy

Leeds Drop Test Method: Results

Materials: Glass Ballotini (90 – 200 µm), Glass Plate (5 mm in diameter), Steel Plate (5 mm in diameter)

Interactions:

- 1) Silanised Glass Ballotini vs Silanised Glass Ballotini/Plate (SGB-SGB)
- Silanised Glass Ballotini vs Non-Silanised Glass Ballotini/Plate (SGB-NSGB)
- 3) Silanised Glass Ballotini vs. Steel Plate (SGB-SP)

#### Drop Test Results

SGB – SGB	SGB – NSGB	SGB – SP
$\mathbf{G}_{SGB-SGB} = 27.4  \mathbf{\acute{g}}mJ/m^2$ မွဲ	$G_{SGB-NSGB}=20.6$ é $mJ/m^2$ မွဲ	$\mathbf{G}_{SGB-SP} = 24.4  \mathbf{\acute{g}} m J / m^2 \mathbf{\acute{g}}$















### Flowability by FT4 Effect of Particle Size: Material

- q Two size classes of glass ballotini were chosen:
  - $\vee$  425 500 µm (on the left)
  - $\vee$  850 1000  $\mu$ m (on the right)





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Three mixtures are considered as follow based on number ratio q 10% (425 – 500 μm) & 90% (850 – 1000 μm) referred to 10S\_90L q 50% (425 – 500 µm) & 50% (850 – 1000 µm) referred to 50S\_50L q 90% (425 – 500 µm) & 10% (850 – 1000 µm) referred to 90S\_10L 905\_10L 105\_90L 50S\_50L Mid Plane **Surface** Mid Plane Surface Surface Mid Plane







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Flowability Effect of Particle Adhesion: Downward Test Results













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### Flowability Effect of Particle Adhesion: Downward Test Results

Number Fraction **Number Fraction** Flow Energy [mJ] NSGB [%] SGB [%] Flow Energy [mJ] 08 08 09 132.3 137.4 138.5 145.9 148.7 Number Fraction of Non Adhesive Glass Beads [%]











## Manufacturability Index for Powder Flow

The Approach of Capece et al.\*

Flow Function and Granular Bond Number For Multi-Component Powder Bed

$$ff_{c,mix} = \boldsymbol{a} \left( Bo_{g,mix} \right)^{-b}$$

$$Bo_{g,Mix} = \bigotimes_{\substack{\boldsymbol{c} \in \mathbf{a} \\ \boldsymbol{c} \in i=1}}^{\mathbf{m}^{N}} \bigotimes_{j=1}^{N} \frac{w_{ij}}{Bo_{g,ij}} \stackrel{\mathbf{o}^{-1}}{\overset{\mathbf{o}}{\overset{\mathbf{o}}{\mathbf{c}}}}$$

*w<sub>ij</sub> is the interaction weighting factor* 

where  $\alpha$  and  $\beta$  are the fitting parameters

 $\alpha$  is the flow function at the cohesive-non-cohesive boundary (Bo<sub>g,mix</sub>=1)

$$Bo_{g,ij} = \frac{F_{ad,ij}}{W_{ij}}$$

$$w_{ij} = f_{SA,i} f_{SA,j}$$

$$W_{ij} = \frac{2W_i W_j}{W_i + W_j}$$

f<sub>SA</sub> is the fractional surface area that gives the likelihood that the two material (i and j) come into contact

\*Capece et al. (2015), Powder Technology 286 561-571











## Elutriation Segregation (Dr W. Nan)



Aspects under investigation:

Ø Effect of the depth of filling vessel

Ø Effect of inlet ratio

Ø Effect of size ratio and density ratio













### **Simulation Parameters**

Parameters	Basic Value	Value range
Geometry		
Length (mm), L	10	-
Depth (mm), H	60	30-180
Width (mm), W	2	-
Inlet ratio, IR	0.6	0.4-1.0
Gas (air)		
Density (kg/m³), <b>ρ</b> <sub>f</sub>	1.2	-
Viscosity (Pa·s), $\mu_f$	1.8×10 <sup>-5</sup>	
Particle		
Diameter (mm), d <sub>p</sub>		
Fine particle, d <sub>p,f</sub>	0.1375	-
Coarse particle, d <sub>p.c</sub>	0.275	0.275, 0.55
Density (kg/m³), <b>ρ</b>		
Fine particle, d <sub>p,f</sub>	1300	-
Coarse particle, d <sub>p,c</sub>	1300	1300, 7800
Volume fraction of fine particle, x <sub>f</sub>	0.1	-
Poisson's ratio, <b>v</b>	0.3	
Shear modulus (MPa), G	10	-
Restitution coefficient, e	0.42	
Friction coefficient, µ	0.5	-













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#### Effect of Inlet Ratio

#### IR=0.4 (a-c), IR=0.6 (d-e), IR=0.8 (f-h) and IR=1.0 (j-k)



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#### Effect of the inlet ratio on the vertical segregation index















# Mixing and Segregation













# Concluding remarks



- develop the science base for understanding of particle surfaces, structures and bulk behaviour to address physical, chemical and mechanical properties and behaviour during processing and storage
- develop formulation science to link molecule to manufacturability (through experimental characterisation and numerical modelling)
- establish methodologies to formulate new materials through developing functional relationships, considering the limits and uncertainties
- Develop a software tool for prediction and optimisation of manufacturability and stability of advanced solids-based formulations

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